

$$I = K_1 \int_{z_f}^{z_i} \frac{V'}{(\rho)^{1/2} V} dz \quad (19)$$

with the condition  $x = l$ . For the lifting entry with minimum heat yielded in the critical zone (denoting by  $K_2$  another constant) one must find the minimum of the functional

$$I^* = K_2 \int_{z_f}^{z_i} \frac{V V'}{(\rho)^{1/2}} dz \quad (20)$$

with the same condition. Both problems may be solved in this manner.

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## Laminar Boundary Layer in Noncentered Unsteady Waves

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PREVIOUS analyses<sup>1,2</sup> have considered the laminar wall boundary layer developed within unsteady simple waves which are centered. The present Note concerns the influence of noncentered wave forms which typically occur in practice. A more detailed account is given in Ref. 3.

Figure 1 shows the straight-line mathematical characteristics in the distance-time or  $x, t$  plane for inviscid flow generated by simple expansion or compression waves.<sup>4</sup> The wavehead moves at constant sound speed  $a_0$  towards  $-x$  into uniform, stationary, perfect gas of constant specific heat ratio  $\gamma$ . The relation  $(\gamma - 1)u_e/2 + a_e = a_0$  applies locally, and flow properties are constant along the straight characteristics which have slopes  $dx/dt = u_e - a_e = u_e/\beta - a_0$  where  $u$  = velocity along  $x$ ,  $a$  = sound speed,  $\beta = 2/(\gamma + 1)$ , and subscripts  $e$  and  $0$  denote inviscid flow and gas ahead of the wave, respectively. The first derivatives of the flow properties are assumed to be initially discontinuous, i.e., to be nonzero immediately after the wavehead (cf. Fig. 2). This requires that the wave be generated with nonzero initial acceleration of the gas (say by suitable piston motion or diaphragm rupture). It then follows<sup>3</sup> that the wavehead first derivatives (subscript  $H$ ) satisfy  $(\partial p/\partial t)_H = a_0(\partial p/\partial x)_H = -\gamma\beta p_0/t$  and  $(\partial u_e/\partial t)_H = a_0(\partial u_e/\partial x)_H = -\beta a_0/t$ . Thus the wavehead first derivatives at any  $x$  [say  $(\partial p/\partial t)_H$  as measured from Fig. 2] automatically define the corresponding time  $t$  and thus uniquely locate the origin of  $x, t$  along the wavehead path. The preceding wavehead relations for noncentered waves apply throughout the entire flow within centered waves.

In Fig. 1,  $e$  is the  $x$ -axis intercept of the straight characteristic through  $x, t$  and also represents the  $x$  displacement of the local particle at  $x, t$  from its position in a centered wave for given velocity  $u_e$ . To any point  $x, t$  there corresponds a unique value of  $e$  determined only by  $u_e$ , i.e.,  $(x - e)/t = u_e/\beta - a_0$ . The noncentered flow is thus completely defined by specifying  $e(u_e)$ . It can be shown<sup>3</sup> that  $de/du_e$  as well as  $e$  must vanish at the

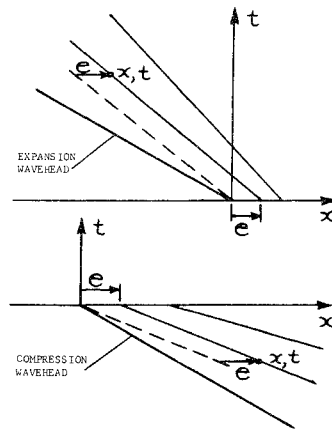


Fig. 1 Distance-time or  $x, t$  diagram of straight characteristics for simple noncentered waves.

wavehead. In general,  $e$  may be  $\geq 0$ . Thus a constant acceleration piston gives  $e > 0$  for compression waves and  $e < 0$  for expansion waves. In experiments with simple waves  $e(u_e)$  can be determined from a record of  $u_e(t)$  or  $p_e(t)$  obtained at any  $x$  location.<sup>3</sup> For example, the measured pressure-time history of Fig. 2 for a diaphragm-generated expansion wave gives the determination of  $e(u_e)$  shown in Fig. 3.

If  $e$  is regarded as a function of  $x$  and  $t$  a new independent variable  $s(x, t)$  can be defined as  $s = 1 + x/a_0 t - e/a_0 t = s^* - e/a_0 t$ .  $s$  provides a local conical similarity for the inviscid flow in noncentered waves analogous to  $s^*$  for centered waves (where  $e \equiv 0$ ). With centered waves  $s^*$  is the ratio of the  $x$  distance of any point  $x, t$  from the wavehead to the distance of the wavehead from the wave focal point. In terms of  $s$  the inviscid flow variables are given by  $u_e = \beta a_0 s$  and  $(p_e/p_0)^{\epsilon/\gamma\beta} = (\rho_e/\rho_0)^{\epsilon/\beta} = (T_e/T_0)^{1/2} = a_e/a_0 = 1 - \epsilon s$ , where  $\rho$  is density,  $T$  is absolute temperature, and  $\epsilon = (\gamma - 1)/(\gamma + 1)$ .  $s$  is  $> 0$  for expansion waves and  $< 0$  for compression waves; its magnitude increases monotonically from zero at the wavehead where  $x = -a_0 t$  and  $e = 0$ . Although the magnitude of  $e/a_0 t$  will typically be small,  $e$  itself is unrestricted.

### Transformation and Solution of Boundary-Layer Equations

The  $T$ ,  $\rho$ ,  $p$ , and  $u$ -velocity fields outside the gas boundary layer are assumed to be those of the noncentered wave discussed. The initial gas boundary layer ( $y \geq 0$ ,  $y$  = distance normal to wall) is described by the customary approximations for two-dimensional, unsteady, compressible laminar boundary layers with heat transfer. Gas viscosity  $\mu$  is assumed proportional to  $T$ ; local  $\rho\mu$  is thus proportional to  $p = p_e(x, t)$ . Heat transfer also produces a thin thermal boundary layer in the homo-

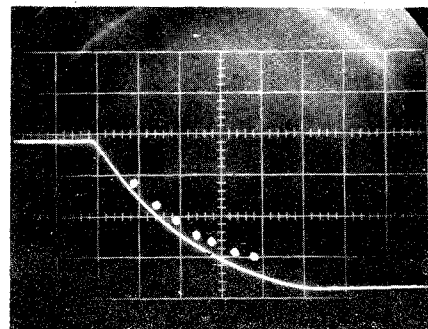


Fig. 2 Oscilloscope trace of sidewall static pressure vs time for expansion wave. 10 psi/cm vertical and 0.5 msec/cm horizontal. Dots indicate centered-wave values. Air with  $p_0 = 85$  psi,  $T_0 = 74^\circ\text{F}$ . Kistler 603A transducer 3 ft from diaphragm. Tube is  $1\frac{1}{2}$  in.  $\times$  5 in. cross section. Flow discharges to room through choked 1 in.  $\times$  5 in. slot orifice plate at tube end.

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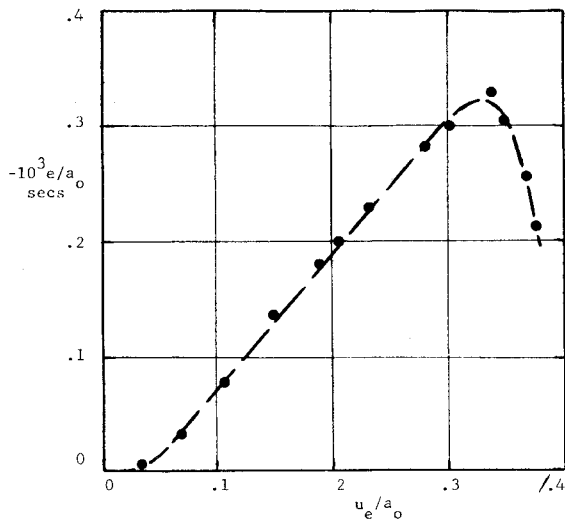


Fig. 3 Function  $e(u_e)$  determined from pressure record of Fig. 2.

geneous wall ( $y \leq 0$ ). Temperature  $\theta$  in the wall is governed by the approximate heat-conduction equation  $\partial\theta/\partial t = \alpha\partial^2\theta/\partial y^2$ , where  $\alpha$  = wall thermal diffusivity. The assumed  $y$  boundary conditions are: at  $y = \infty$ ,  $u = u_e$  and  $T = T_e$ ; at  $y = 0$ ,  $u = v$  (= gas velocity along  $y$ ) = 0 and  $T = \theta = T_w(x, t)$ ; and at  $y = -\infty$ ,  $\theta = T_0$ . The wall surface temperature  $T_w(x, t)$  is unknown, and its determination in the over-all solution requires matching local gas and wall heat-transfer rates at  $y = 0$ , i.e.,  $q_w = -k_w(\partial T/\partial y)_{y=0} = -k_B(\partial\theta/\partial y)_{y=0}$  where  $k$  is thermal conductivity and subscripts  $B$  and  $W$  denote wall material and gas conditions at  $y = 0$ , respectively. At the wavehead the gas is at rest and  $\theta = T = T_0$ .

The governing equations are transformed in terms of new independent and dependent variables; the continuity equation is used to eliminate  $v$  from the  $x$ -momentum and gas energy equations. The new independent variables are  $s$ ,  $t' = t$ , and a normal coordinate  $\eta$  defined by  $\eta = [a_0/v_0(x + a_0t - e)]^{1/2} \times \int_0^y (\rho/\rho_0) dy$  for  $y > 0$  and  $\eta = -y[a_0/\alpha(x + a_0t - e)]^{1/2}$  for  $y < 0$ , where  $v = \mu/\rho$ . The new dependent variables are  $F$ ,  $G$ , and  $H$ , defined by  $u = u_e\partial F/\partial\eta$ ,  $T = T_w + (T_e - T_w)G$ , and  $\theta = T_w + (T_0 - T_w)H$ . The transformed equations<sup>3</sup> constitute three nonlinear partial differential equations involving  $F$ ,  $G$ ,  $H$ , and  $T_w(s, t')$ , and an algebraic relation involving  $T_w$  and surface values of  $\partial G/\partial\eta$  and  $\partial H/\partial\eta$ . The  $t'$  dependence appears only in a local inverse-time parameter  $\omega = (\beta/t')de/du_e$  which depends implicitly on  $s$  as well as on  $t'$ .

$\omega$  must vanish at the wavehead and can be considered small compared to unity in the initial flow region.<sup>3</sup> The dependent

functions can then be expressed as asymptotic series expansions in ascending powers of  $\omega$  with coefficients  $Y_i(s, \eta)$ . For the initial flow region  $s$  is also small, and the  $Y_i$  can in turn be expressed as power series expansions in  $s$ . Thus  $\partial F/\partial\eta$ ,  $G$ , and  $H$  are represented by  $Y = \sum \omega^i Y_i = \sum \sum \omega^i Y_{ij} s^j$  where  $Y_{ij} = Y_{ij}(\eta)$  and  $i, j$  take values 0, 1, 2, .... Similarly for the surface temperature,  $T_w/T_0 = \sum \omega^i B_i = \sum \sum \omega^i B_{ij} s^j$  where  $B_i = B_i(s)$  and  $B_{ij} = \text{constant}$ . Substitution into the transformed equations then leads to a sequence of linear ordinary differential equations for  $Y_{ij}$  (and algebraic equations for  $B_{ij}$ ) of the form<sup>3</sup>  $Y_{ij}'' + (z/2)Y_{ij}' - (i+j+1)Y_{ij} = \bar{Y}_{ij}$  where  $Y_{ij}' = dY_{ij}/dz$ , and  $Y_{ij}$  represents  $F_{ij}$ ,  $G_{ij}$ , or  $H_{ij}$  with  $z = \eta$ ,  $\sigma^{1/2}\eta$ , or  $\eta$ , respectively. The boundary conditions are  $Y_{ij}(0) = Y_{ij}(\infty) = 0$  except for  $Y_{00}(\infty) = 1$ .

### Results and Discussion

The function  $\bar{Y}_{ij}$  denotes nonhomogeneous terms generally dependent on lower order functions and implicitly on  $Y_{ij}'(0)$ . The general solutions to the homogeneous equations are expressible in terms of repeated error function integrals. However, for  $j \geq 1$  the  $\bar{Y}_{ij}$  are sufficiently complicated that numerical methods are appropriate. The present consideration was limited to the zero-order solution ( $i = 0$ ) and to the leading terms in  $\omega$  and  $\omega^2$  ( $i = 1$  and  $2$ ,  $j = 0$ ).

The zero-order equations are identical to those of Ref. 2 for the centered-wave problem with finite  $k_B$  or variable  $T_w$ . Consequently, the zero-order solution is given by the centered wave solution with the centered wave variables  $s^*$  and  $\eta^*$  replaced by  $s$  and  $\eta$ . Although the zero-order solution partially accounts for noncentered wave effects through  $s$  and  $\eta$ , a more complete solution requires higher-order terms in  $\omega$ . The leading terms in  $\omega$  and  $\omega^2$  are obtainable in closed form as follows<sup>3</sup>:  $Y_{10} = (z^2/2)(1 + z^2/12) \operatorname{erf} c(z/2) - (5z/6\pi^{1/2})(1 + z^2/10) \exp(-z^2/4)$ , and  $Y_{20} = -(z^2/2)(1 + z^2/4 + z^4/120) \operatorname{erf} c(z/2) + (z/30\pi^{1/2})(129/8 + 7z^2 + z^4/4) \exp(-z^2/4)$  where  $Y_{i0}$  represents  $F_{i0}$ ,  $G_{i0}$ , or  $H_{i0}$  with  $z = \eta$ ,  $\sigma^{1/2}\eta$ , or  $\eta$ , respectively. The solutions for  $Y_{10}$  and  $Y_{20}$  are plotted in Fig. 4 along with the leading term of the zero-order solution  $Y_{00} = 1 - (1 + z^2/2) \operatorname{erf} c(z/2) + z\pi^{-1/2} \exp(-z^2/4)$ . As expected, the functions and their initial slopes become smaller as  $i$  increases. The initial slopes, which determine surface heat transfer and shear stress, have the values  $Y_{00}'(0) = 2/\pi^{1/2}$ ,  $Y_{10}'(0) = -5/6\pi^{1/2}$ ,  $Y_{20}'(0) = 129/240\pi^{1/2}$ .

For the  $B_{ij}$ ,  $B_{i0} = 0$  except for  $B_{00} = 1$ , and  $B_{i1} = 0$  for  $i \geq 1$ . The result for  $T_w$  is  $T_w/T_0 = 1 + B_{01}s + B_{02}s^2 + \dots + O(\omega s^2)$ . Thus the noncentered wave influence on  $T_w$  is largely accounted for by the zero-order solution  $B_0(s)$ . The first term in  $\omega$  is of third order ( $\omega s^2$ ) in the quantities considered small. Considering only first-order terms, the fractional change in  $T_w - T_0$  at given  $x$  and  $t$  caused by the noncentered wave form is  $(T_w - T_w^*)/(T_w^* - T_0) \approx (s - s^*)/s^* = -e/a_0 s^* t = -(1 + u_e/\beta e)^{-1}$ , where  $T_w^*(x, t)$  is the centered-wave solution. For the expansion-wave example of Fig. 3, where  $e < 0$  and  $s > 0$ ,  $T_w$  is thus reduced below  $T_w^*$ . The maximum effect at distances of 3–4 ft from the origin, or  $t$  in the range of approximately 4 to 6 msec, is about 20–25%. The magnitude of the effect will vary approximately as  $1/x$  or  $1/t$ .

The noncentered wave influence on the surface heat-transfer rate  $q_w$  is most readily evaluated for  $k_B = \infty$  ( $T_w = \text{const}$ ) for which  $B_{0j} = 0$  and  $G_{01}'(0) = 0.1507$  (Ref. 1) for  $\sigma = 0.72$ ,  $\gamma = 1.4$ . Considering only leading terms, the fractional change in  $q_w(x, t)$  is given approximately by<sup>3</sup>  $(q_w - q_w^*)/q_w^* \approx [\epsilon/2 + \gamma\beta(1 - a_0/2\gamma u_e) - G_{01}'(0)/G_{00}'(0)]e/a_0 t + \omega G_{10}'(0)/G_{00}'(0)$  in the limit  $k_B = \infty$ , where  $q_w^*(x, t)$  is the centered wave value. For the expansion wave of Fig. 3 both  $e$  and  $\omega$  are negative at small  $s$ . Both right hand terms of  $q_w - q_w^*$  are then positive, so that  $q_w$  is increased over  $q_w^*$  in that case. For  $t$  in the range of 4–6 msec the maximum increase in  $q_w$  is about 10–15% (varying approximately as  $1/x$  or  $1/t$ ). The results for skin friction are qualitatively similar to those for heat transfer but the noncentered wave effects are somewhat larger.<sup>3</sup>

In earlier shock-tube experiments<sup>5</sup> substantial discrepancies

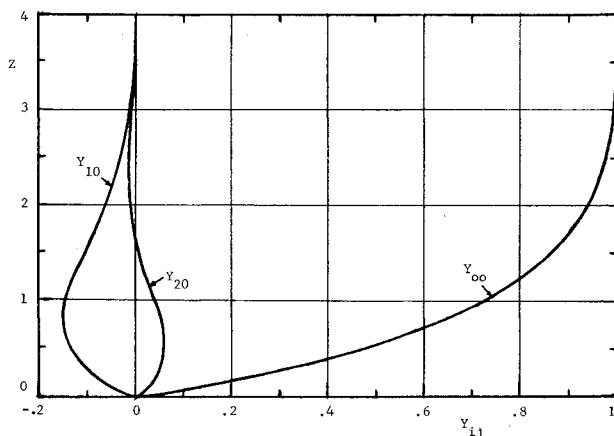


Fig. 4 Functions  $Y_{00}$ ,  $Y_{10}$ ,  $Y_{20}$ .

were observed between measured values of  $T_w$  and  $q_w$  and the laminar boundary-layer theory for centered expansion waves. If the (unmeasured) waveforms were qualitatively similar to that of Fig. 2 then the observed discrepancies are at least qualitatively explained by the predictions of the present analysis.

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## Hot-Wire Coil Probe for High-Speed Flows

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### Nomenclature

$d$	= diameter of wire
$D$	= diameter of coil
$e$	= compensated hot-wire output voltage
$f$	= frequency
$h$	= wire film coefficient of heat transfer
$I$	= hot-wire heating current
$k$	= thermal conductivity of gas
$l$	= length of wire
$M$	= Mach number
$Nu_t$	= $hd/k_t$ = Nusselt number
$Re_{t,d}$	= $(\rho U)_t d / \mu_t$ and $(\rho U)_t D / \mu_t$ , respectively, Reynolds number
$T$	= temperature
$U$	= gas velocity
$\eta$	= wire recovery factor ( $T_w/T_t$ as $I_w \rightarrow 0$ )
$\mu$	= gas viscosity
$\rho$	= gas density

### Subscripts

$\infty$	= freestream value
$d$	= based on wire diameter
$D$	= based on coil diameter
$l$	= local flow value
$w$	= hot wire
$t$	= local total value

### Introduction

CONVENTIONAL hot-wire probes for high-speed flows typically have the wire mounted slack between end supports. This slack minimizes wire breakage, and reduces strain gage

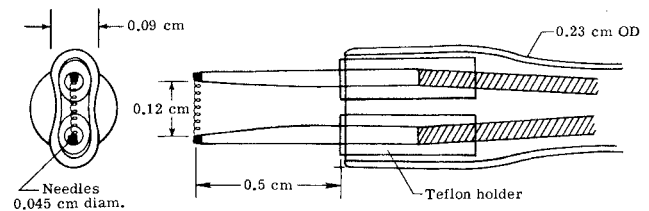


Fig. 1 Hot-wire coil-probe construction.

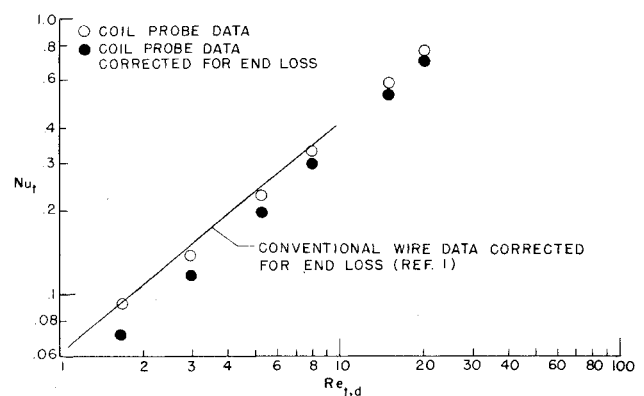
effects.<sup>1</sup> The wire length to diameter ratio and necessary amount of slack depend on the test environment, and are a compromise between end loss effects and strength. For high wire loading the wire may need to be so short that end conduction losses are large. In addition, the large amount of slack needed can result in wire support interference even when the probe is at a small angle to the mean flow.

One possible solution to some of the limitations of a conventional fine-wire probe is the use of a small diameter coil of wire for the probe. The springlike properties of the coil allow a higher length-to-diameter ratio for a given flow and minimize strain gage effects. In addition, the coil is more rugged for sudden flow changes. Since a coil can be mounted straight across the support tips there is less support interference in cross flows.

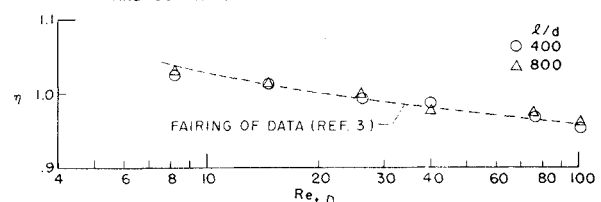
This Note describes such "coil probes" developed for use in a hypersonic helium tunnel. In addition to measuring fluctuating quantities in a boundary layer, these probes were used with a constant temperature anemometer for measuring mean mass flow profiles, and with the constant current anemometer for measuring mean total temperature profiles.

### Probe Construction and Calibration

A small coil of tungsten wire (from a light bulb) was copper plated, stretched across notched needles, and soft soldered to the needle tips. The copper plating between the needles was then removed with nitric acid. The needles were held in a teflon insulator within a small stainless-steel tube. A sketch of a typical probe is shown in Fig. 1. Different size wires and coils were employed with different  $(l/d)$ 's, depending on the flow environ-



a) NUSSLETT NUMBER CALIBRATION OF COIL PROBE ( $l/d = 400$ ,  $d = 0.025$  cm) AND COMPARISON WITH CONVENTIONAL WIRE.



b) WIRE RECOVERY FACTOR CORRECTED FOR END-LOSS.

Fig. 2 Typical hot-wire coil-probe calibrations.

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